

# Gas Adsorption Equilibria Measurements and Correlations

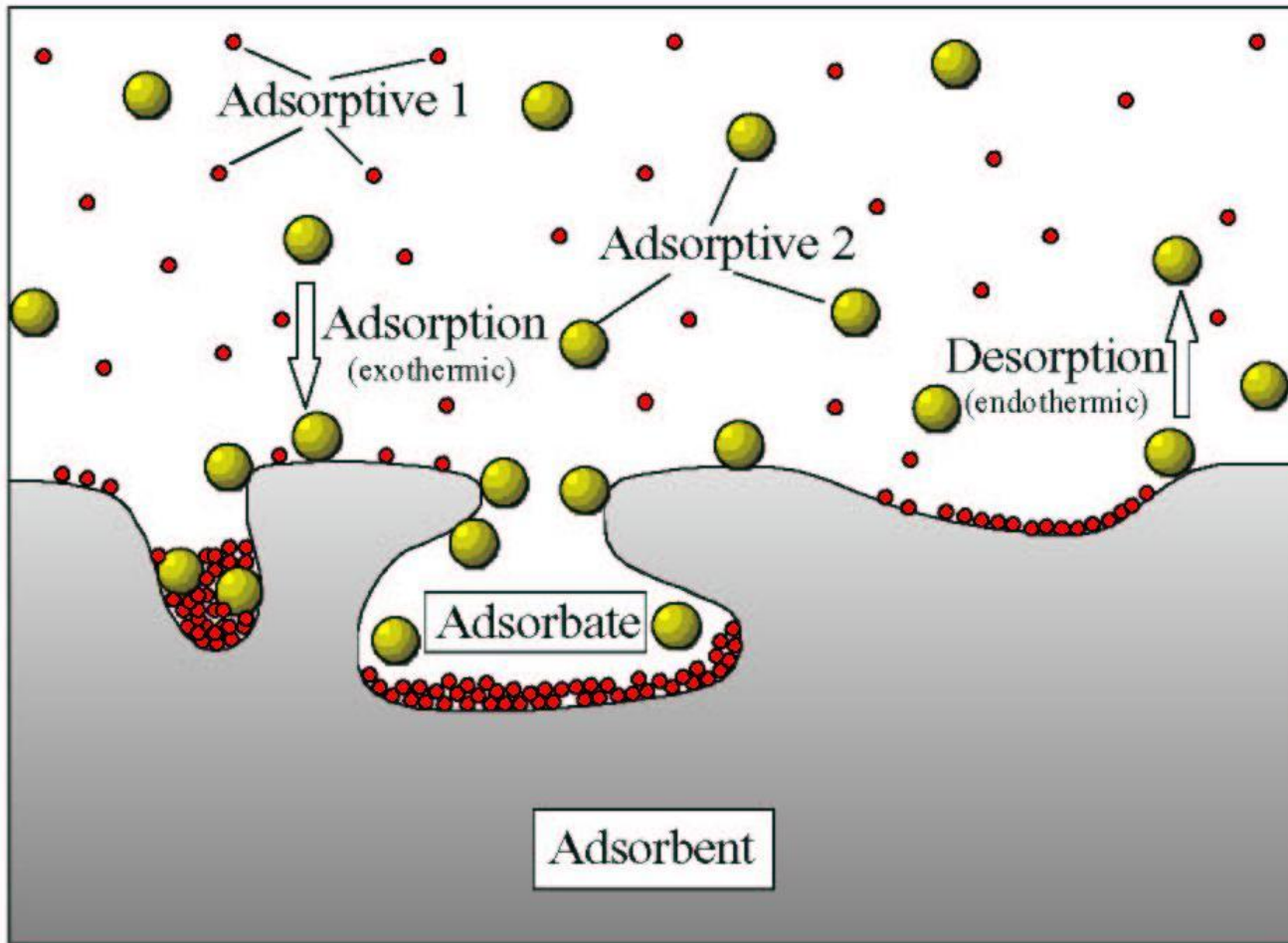
J. U. Keller<sup>1)</sup>, R. Staudt<sup>2)</sup>, W. Zimmermann<sup>1)</sup>

<sup>1)</sup>Inst. Fluid- & Thermodynamik  
Universität Siegen, 57068 Siegen  
E-Mail: keller@ift.maschinenbau.uni-siegen.de

<sup>2)</sup>Inst. Nichtklassische Chemie,  
Universität Leipzig, 04318 Leipzig  
E-Mail: staudt@inc.uni-leipzig.de

## Contents

- 1) Volumetry / Manometry
- 2) Gravimetry
- 3) Hybridmeasurements
- 4) Oscillometrie
- 5) Impedance Spectroscopy
- 6) Calorimetry
- 7) Adsorption Isotherms



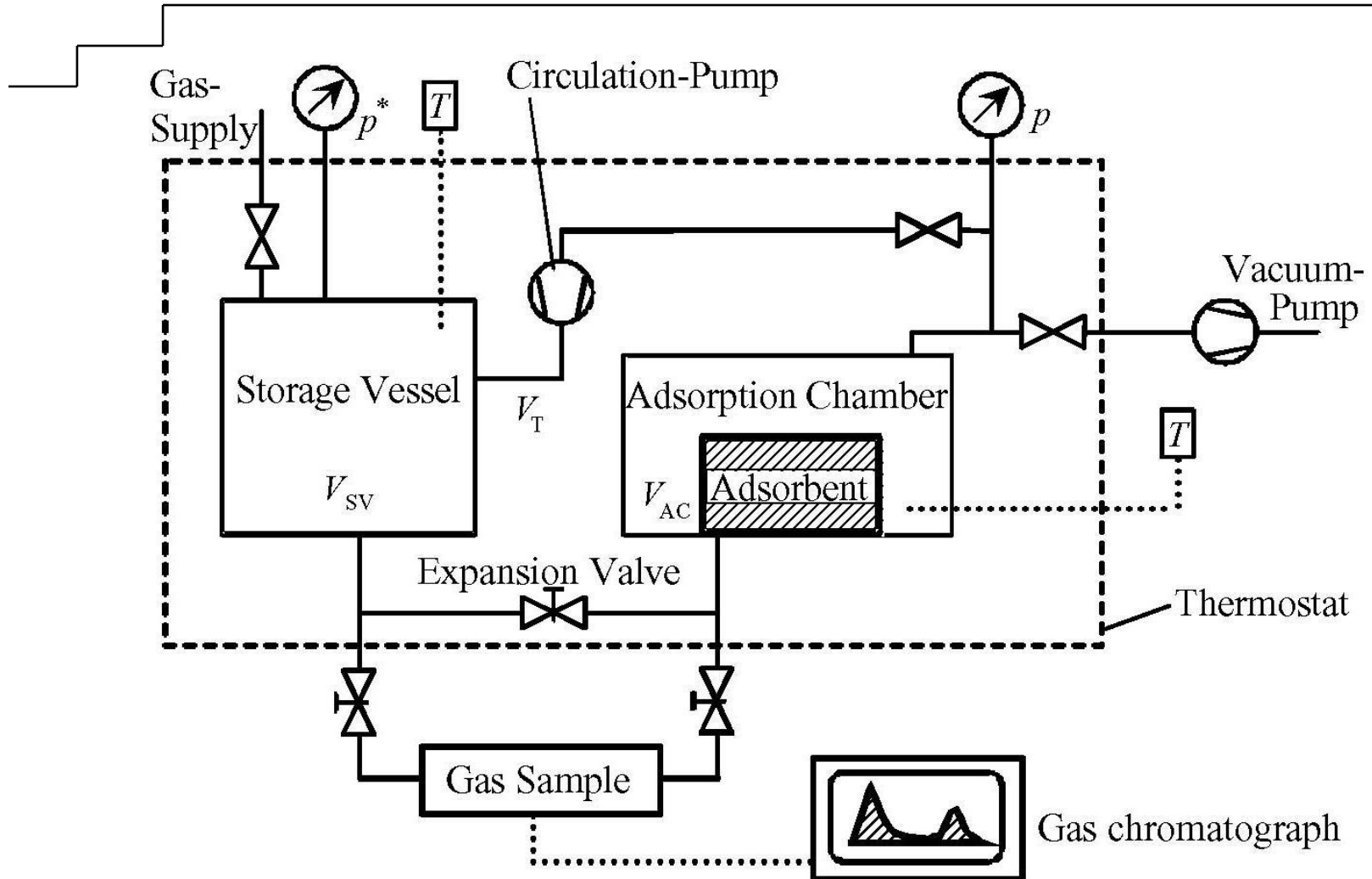
# Adsorption



# Gas Mixture Sorption

## Measurement Methods

		M	G	O	SP	CHR	D	C
Manometry	(M)		++	+	0	++	++	0
Gravimetry	(G)	2		+	0	+	+	0
Oscillometry	(O)	1, V	1, V		0	0	0	0
Spectroscopy	(SP)	(2)	(2)	1, V		-	-	AMA
Chromatography	(CHR)	≥2	≥2	≥2*	-		-	-
Densimetry	(D)	2	2	1, V	-	-		-
Calorimetry	(C)	(1)	(1)	(1)	1	-	-	



**Experimental setup for volumetric-chromatographic measurements of multicomponent gas adsorption equilibria**

Mass balances  $m_i^* = m_i^f + m_i \quad i = 1 \dots N \quad (1)$

Total mass (i)  $m_i^* = w_i^* \rho_i^f(T, p^*, w_1^* \dots w_N^*) V_{SV} \quad (2)$

Adsorptive's mass (i)  $m_i^f = \rho_i^f V_{SV} + V_{AC} - V_S \quad (3)$

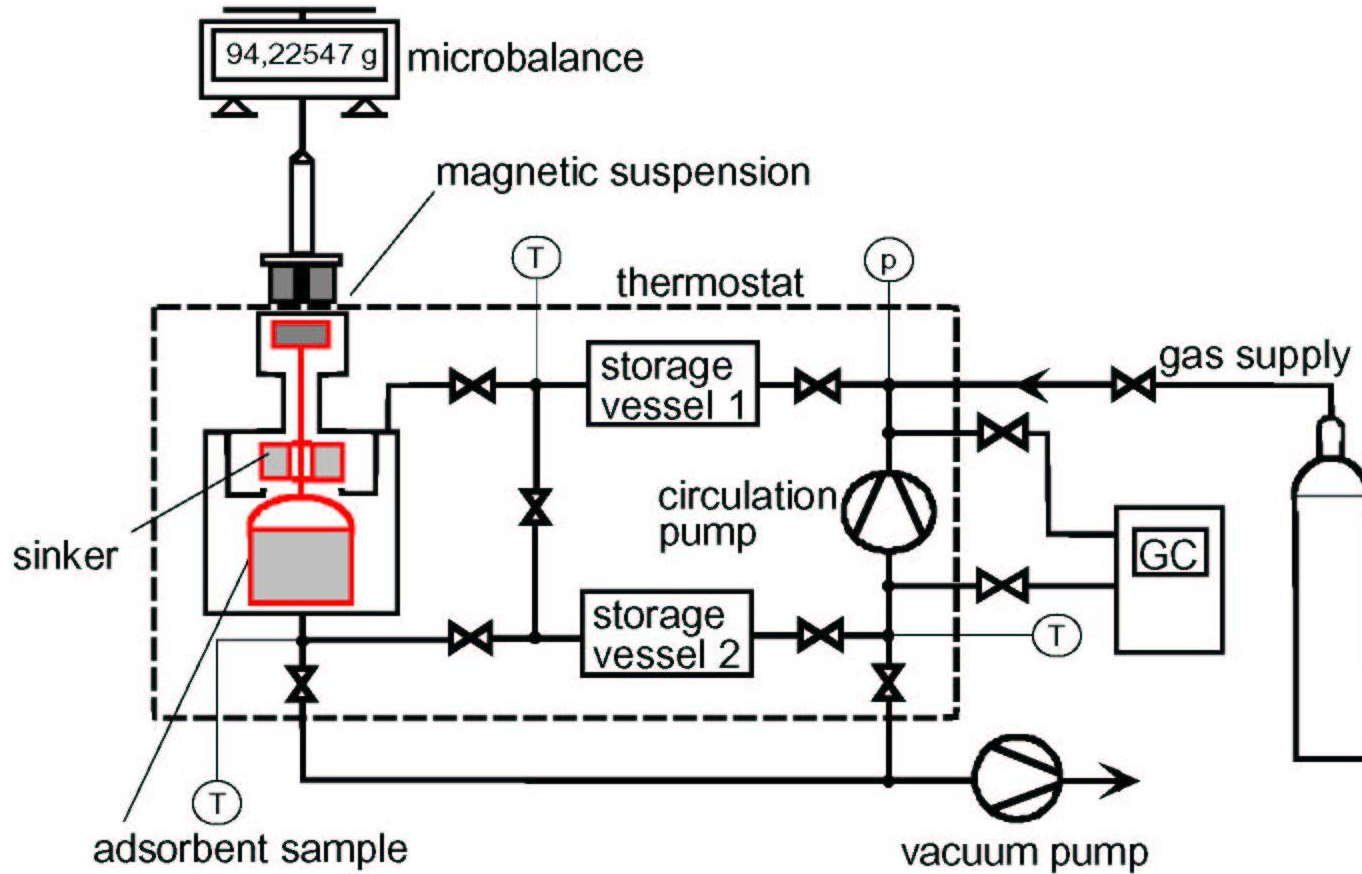
(1-3):  $\underline{\Omega_i = m_i - \rho_i^f V^S} \quad (4)$

$$\Omega_i = \rho_i^* - \rho_i V_{SV} - \rho_i V_{AC}$$

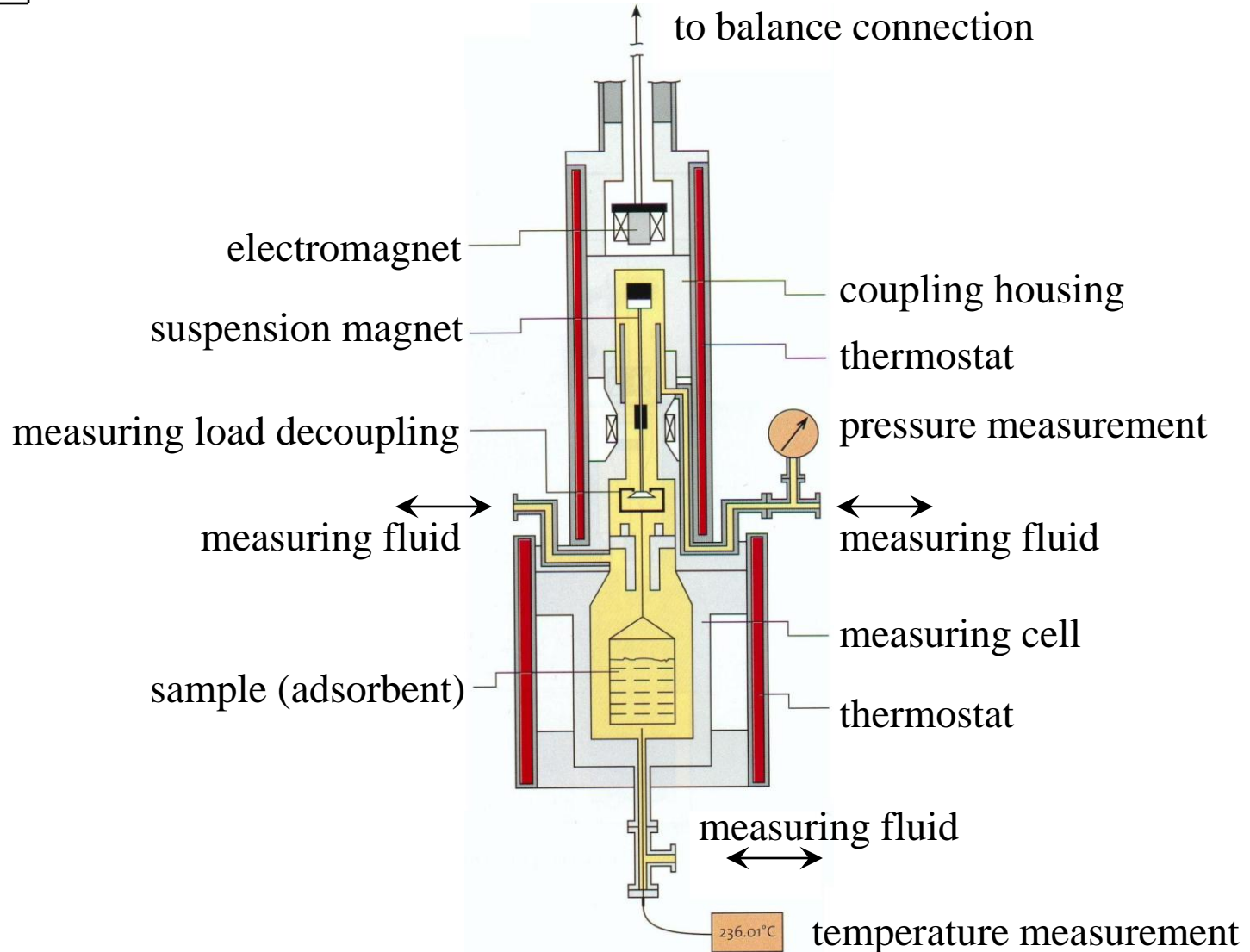
$$\rho_i^f = w_i^f \rho_i^f(T, p, w, \dots w_N), \quad w_i : GC$$

$m_i$  ... Gibbs excess mass

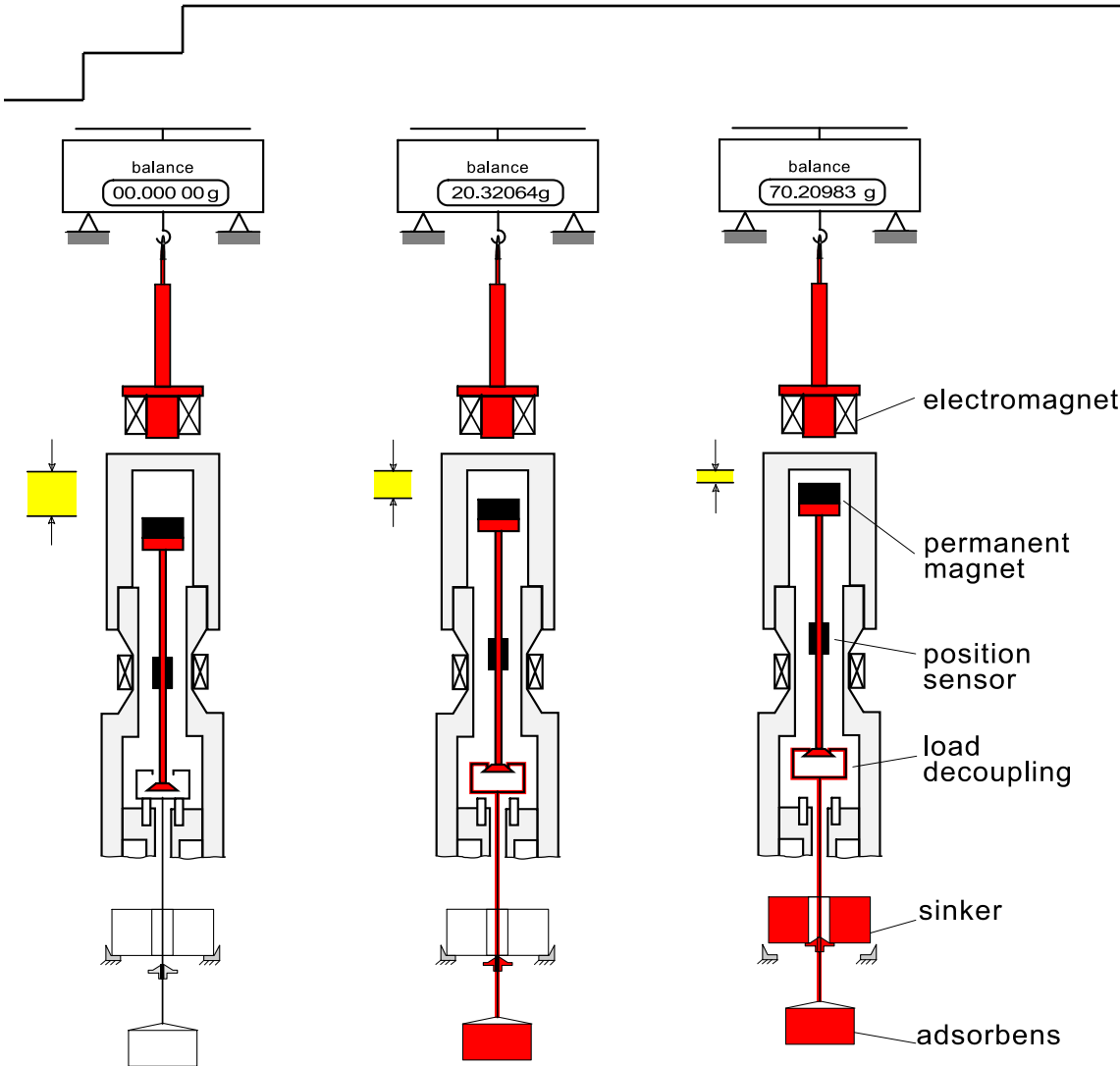
## Volumetry / Manometry



**Schematic diagram of volumetric-gravimetric-chromatographic installation with magnetic suspension balance**



# Sorption measurement (Rubotherm)



# Simultaneous Sorption and Density Measurement (Rubotherm, Bochum, Germany)

zero point  
(tare)

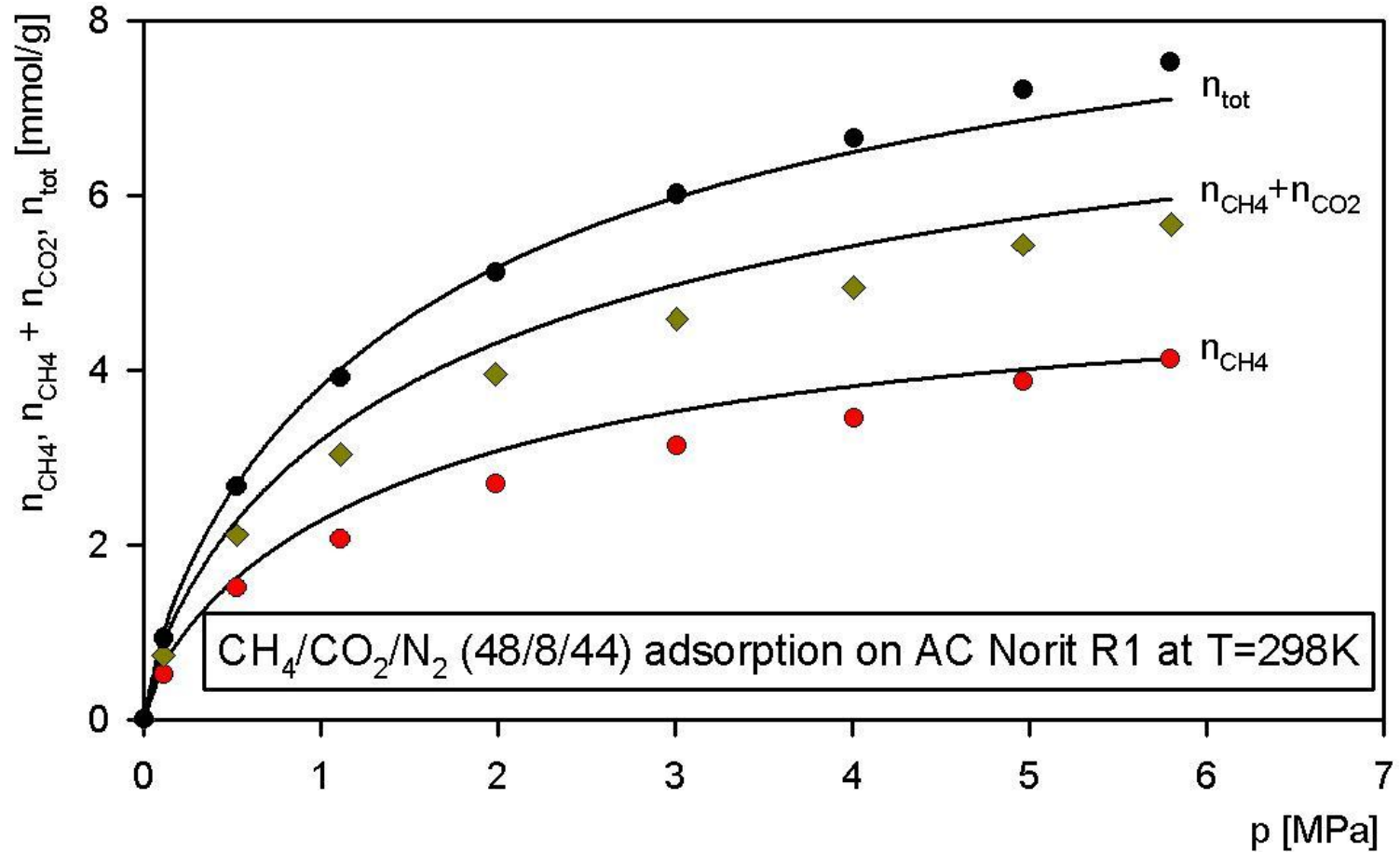
measuring  
point I  
(sorption)

measuring  
point II  
(density)

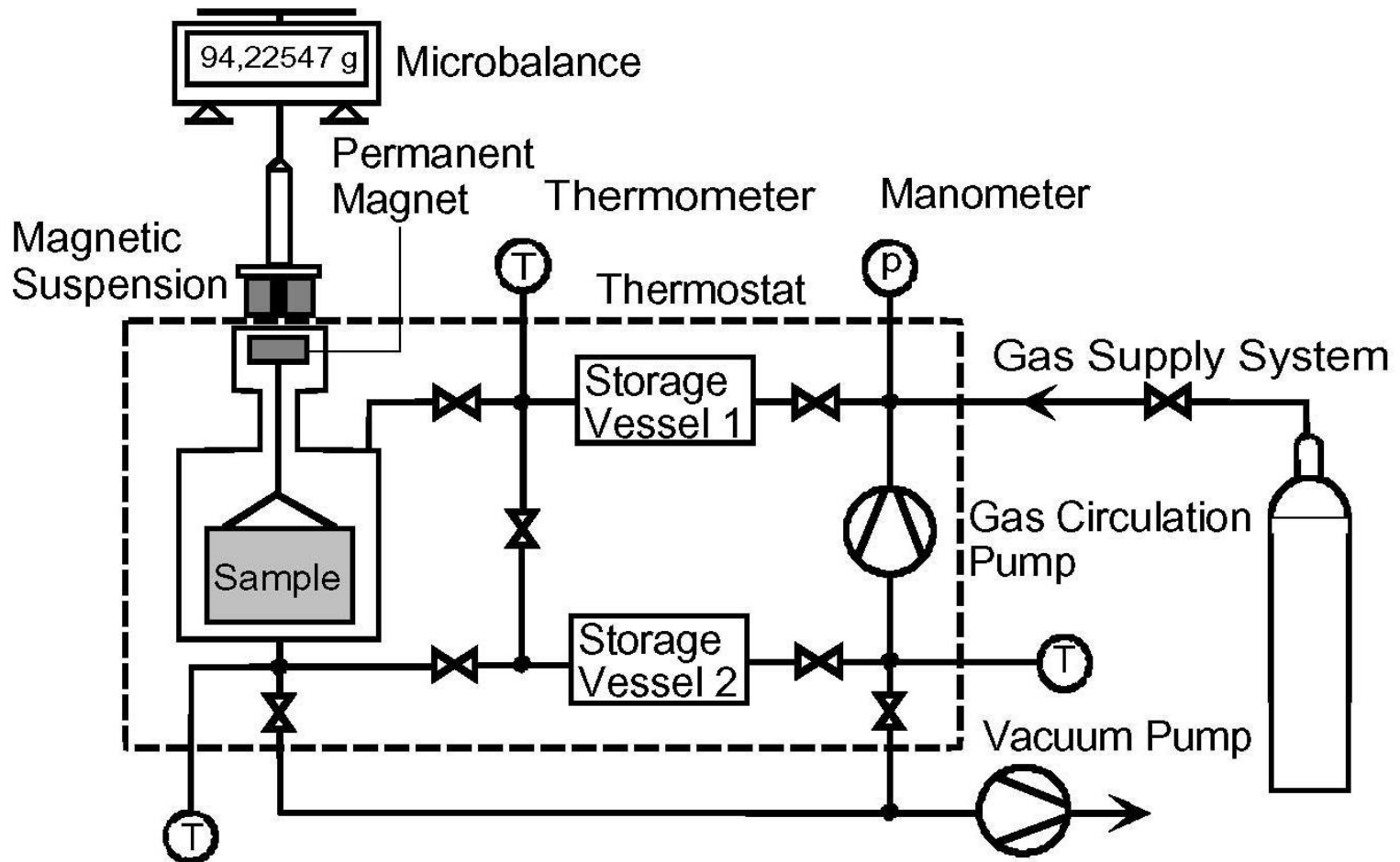




## **Magnetic-Suspension-Balance Instrument (12/96)**



**Prediction of ternary adsorption data with the 2-sites AI**



## Experimental Setup for volumetric-gravimetric measurements

Mass balances

$$m_i^* = m_i^f + \left( 1 + \frac{m_0^s}{m^s} \right) m_i \quad i = 1, 2$$

Micro-balance equation

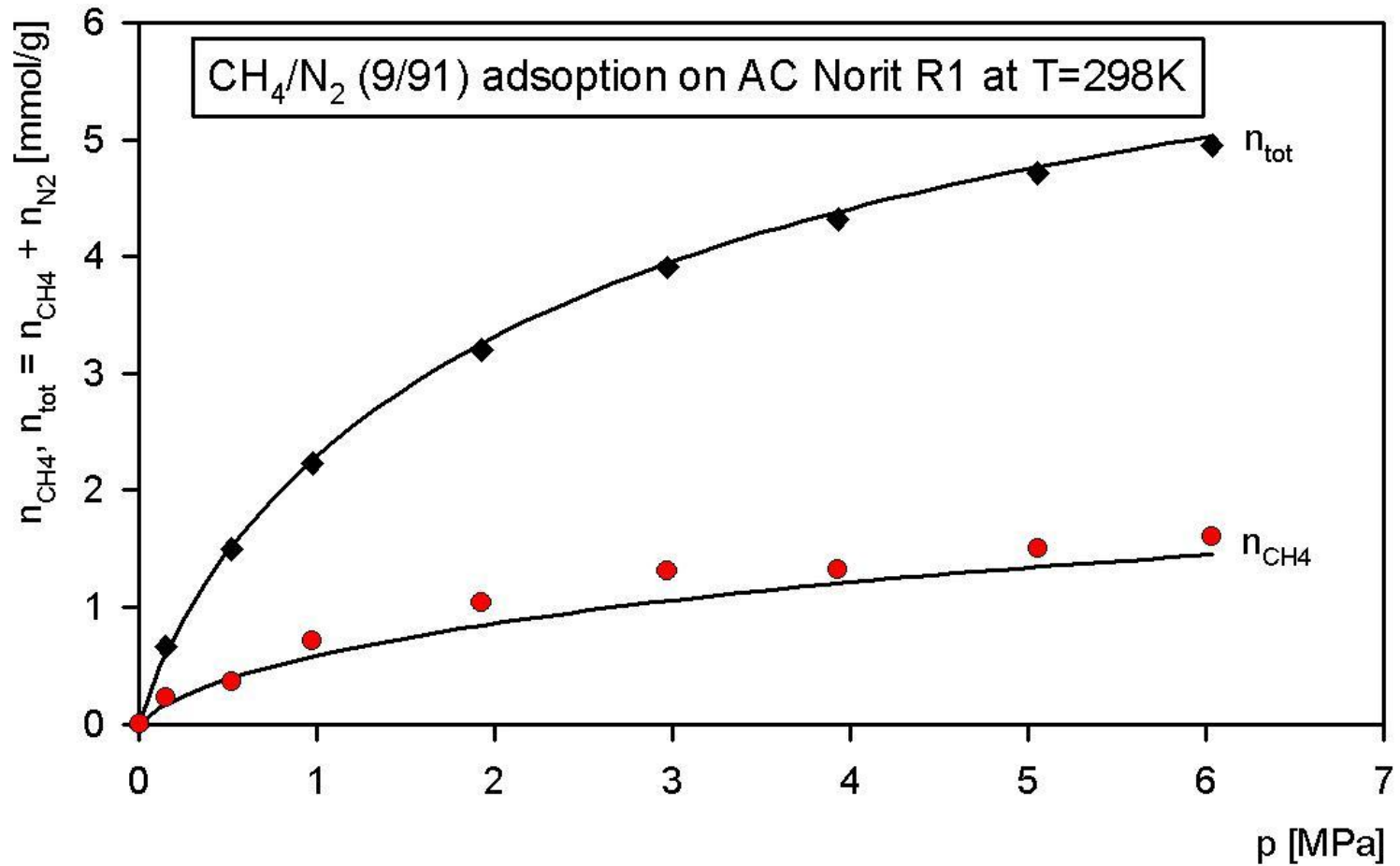
$$\Omega = m_1 + m_2 - V^{\text{as}} \frac{m_1^f + m_2^f}{V^* + V^f}$$

Adsorptive's equation of state

$$\frac{m_1^f}{M_1} + \frac{m_2^f}{M_2} = \frac{p}{ZRT} (V^* + V^f)$$

$$\rightarrow m_1, m_2, m_1^f, m_2^f \dots V^f = V - \left( 1 + \frac{m_0^s}{m^s} \right) V^{\text{as}} \quad \text{if } M_1 \neq M_2$$

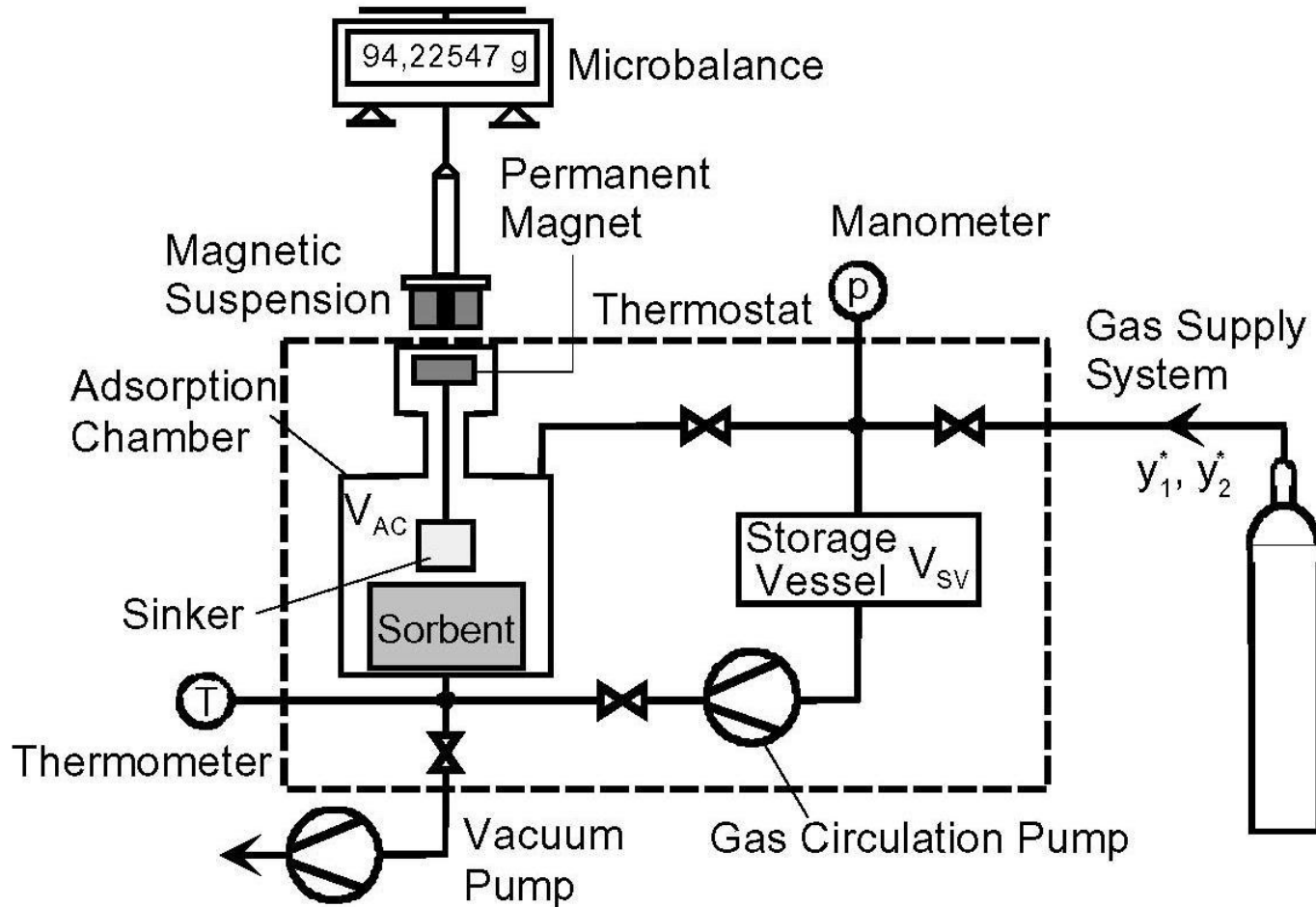
## Volumetric-Gravimetric Measurements of Binary Coadsorption Equilibria



**Prediction of binary adsorption data with the 2-sites AI**



**Coadsorption Instrument  
BEL-Rubotherm, IFT, 2001**



## Installation for DVMs of Binary Coadsorption Equilibria of Premixed Gases $y_1^*, y_2^*$





**Instrument for DVMs of binary coadsorption equilibria  
using a MSB (2) (Rubotherm AG, Bochum)**





**Automated MSB (2) (Rubotherm AG, Bochum)  
for DVMs of binary coadsorption equilibria**

Mass balances  $m_i^a = m_i^* - m_i^f \quad i = 1, 2 \quad (1)$

EOS  $m_i^* = \frac{y_i^* p^* V_{SV}^*}{RTZ^*} M_i \quad Z = Z(p^*, T, y_i^*) \quad (2)$

Sorptive gas masses  $m_1^f + m_2^f = \rho^f (V^* - V^{as}) \quad (3)$   
( $m_1^f, m_2^f$ )

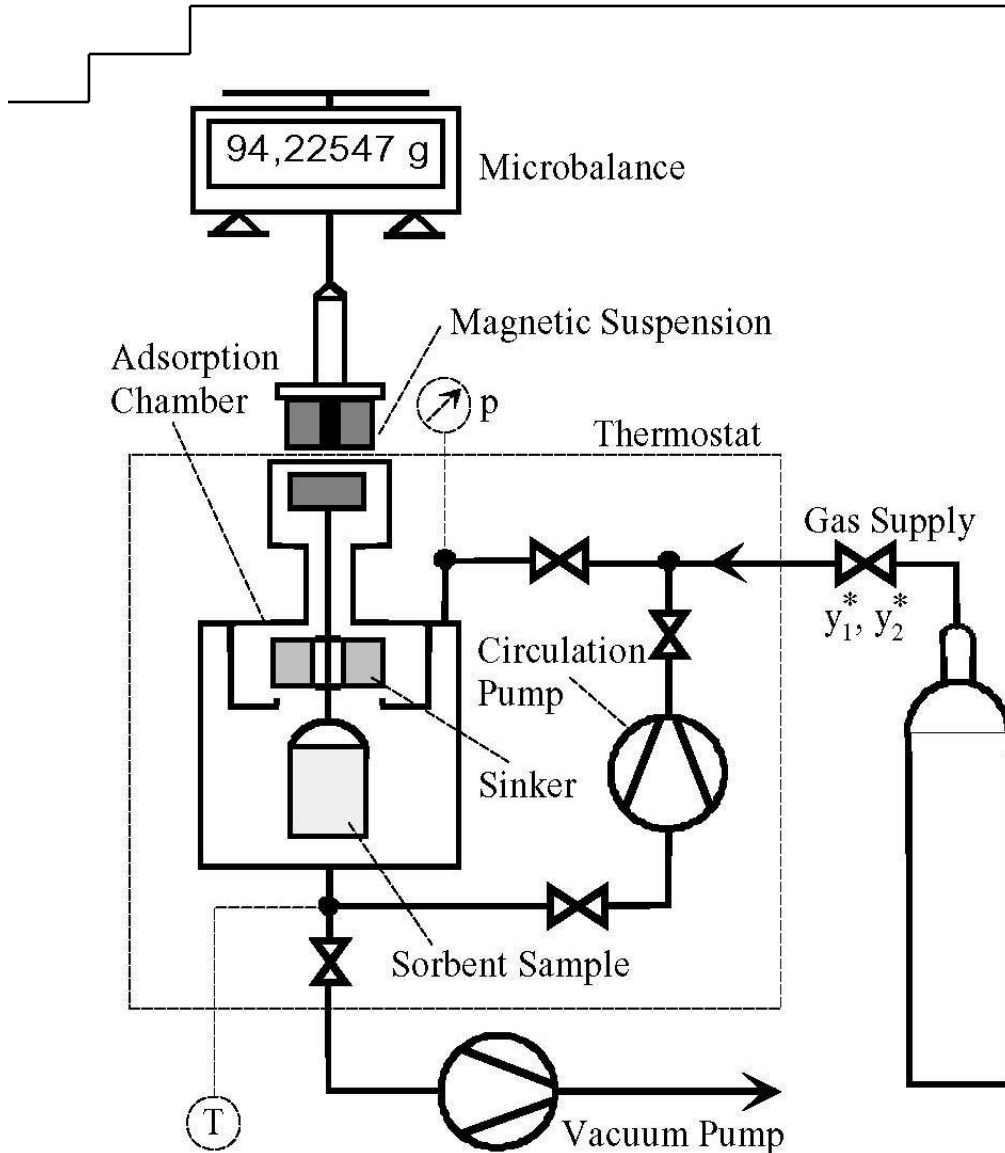
$$\frac{m_1^f}{M_1} + \frac{m_2^f}{M_2} = \frac{p (V^* - V^{as})}{RTZ(p, T, w_i)} \quad (4)$$

---

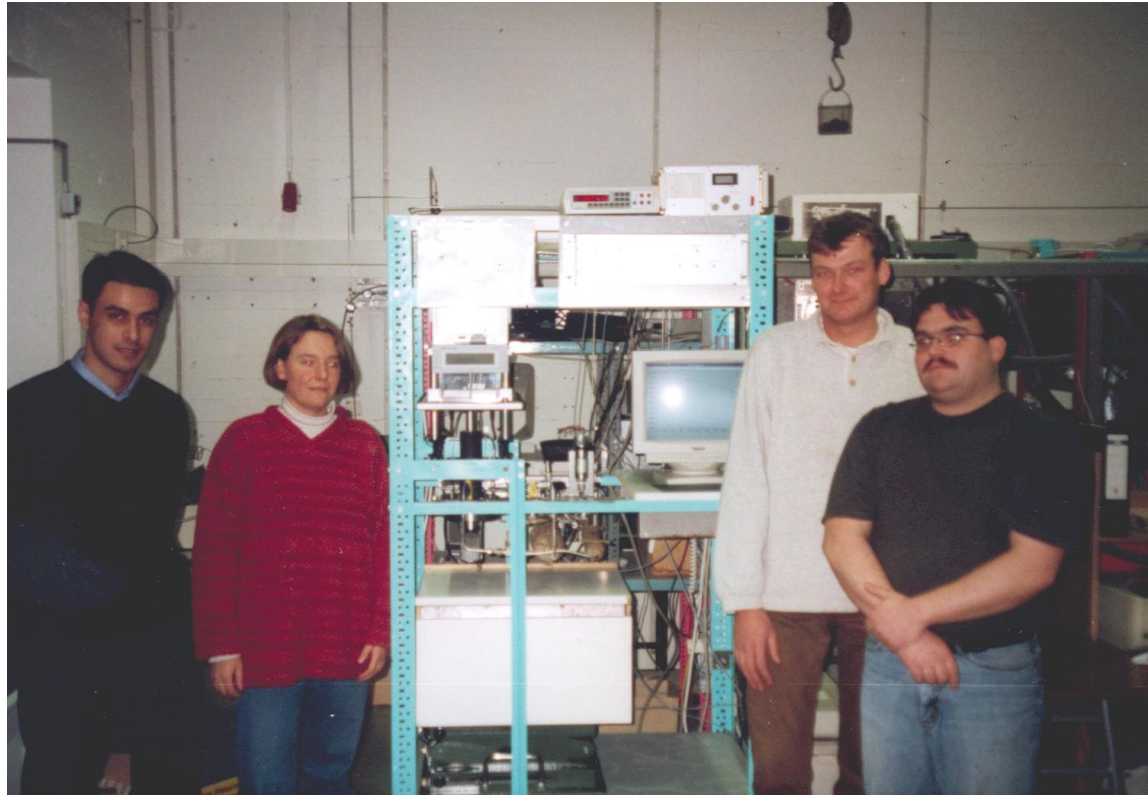

$$w_i = \frac{m_i^f}{m_1^f + m_2^f} \quad i = 1, 2$$

(1 - 4)  $V^{as} = V_{He}^s \quad (5)$

$$m_{iGE}^a = m_i^* - \frac{M_i}{M_i - M_{i+1}} \left( \rho^f - \frac{p M_{i+1}}{RTZ(p, T, w_i)} \right) (V^* - V_{He}^s) \quad (6)$$



## Installation for DGMs of Binary Coadsorption Equilibria of Premixed Gases ( $y_1^*, y_2^*$ )



**First performance of DGMs using a MSB (3)  
on 1998-02-11 in Lab PB-A0126 of IFT/USI**

$$\text{Mass balances} \quad m_i^a = m_i^* - m_i^f \quad i = 1, 2 \quad (1)$$

$$\text{Total gas mass supplied} \quad m^* = m_1^* + m_2^* = m_1^a + m_2^a + m_1^f + m_2^f \quad (2)$$

$$m^* = \Omega + \rho^f V^*$$

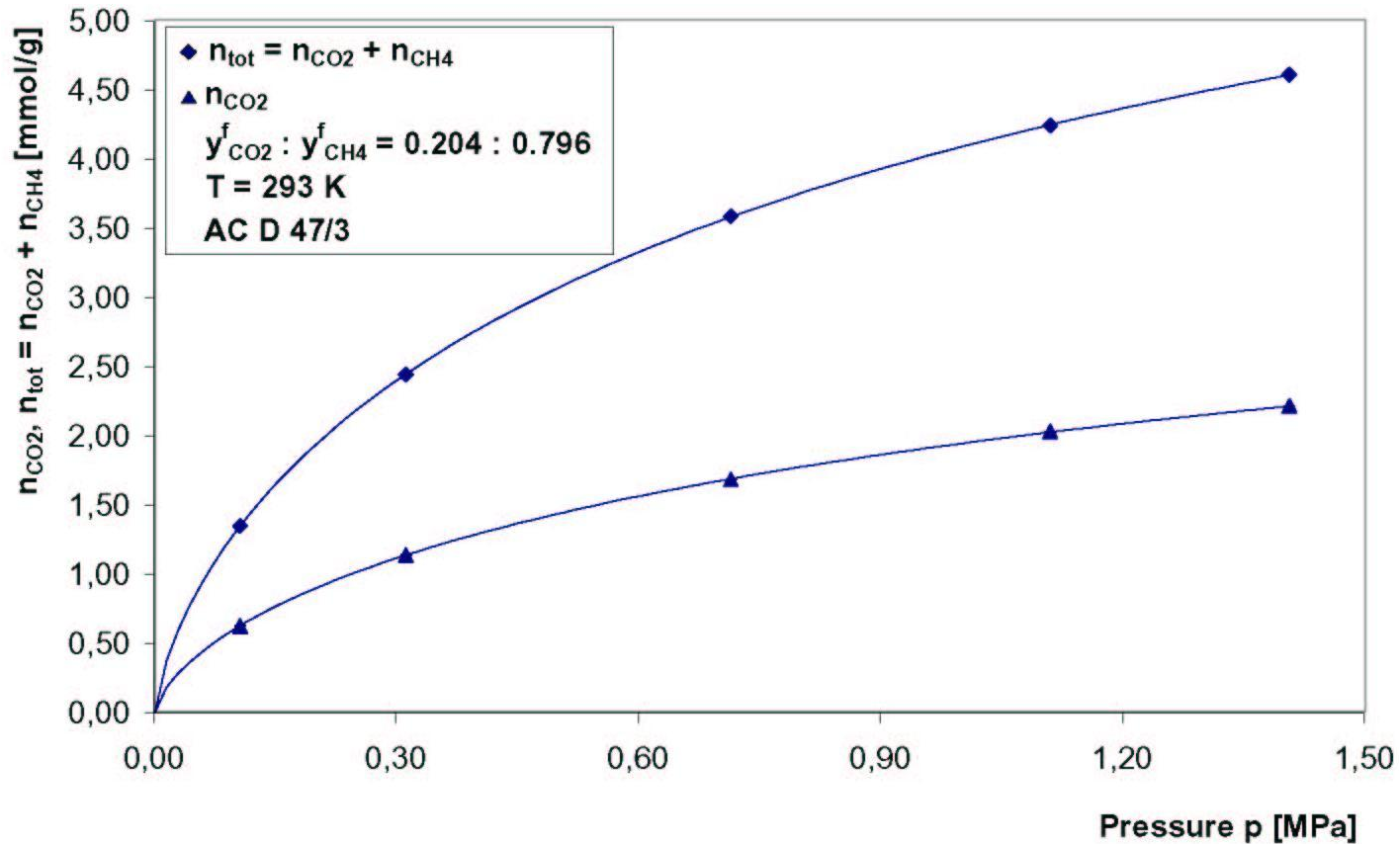
$$m_i^* = w_i^* m^* \quad (2A)$$

$$\text{Sorptive gas masses} \quad m_1^f + m_2^f = \rho^f V^* - V^{\text{as}} \quad (3)$$

$$\frac{m_1^f}{M_1} + \frac{m_2^f}{M_2} = \frac{p V^* - V^{\text{as}}}{RTZ p, T, w_i} \quad (4)$$

$$(1, 2A, 3, 4) \quad V^{\text{as}} = V_{\text{He}}^s \quad (5)$$

$$m_{i\text{GE}}^a = m_i^* - \frac{M_i}{M_i - M_{i+1}} \left( \rho^f - \frac{p M_{i+1}}{RTZ p, T, w_i} \right) V^* - V_{\text{He}}^s \quad (6)$$

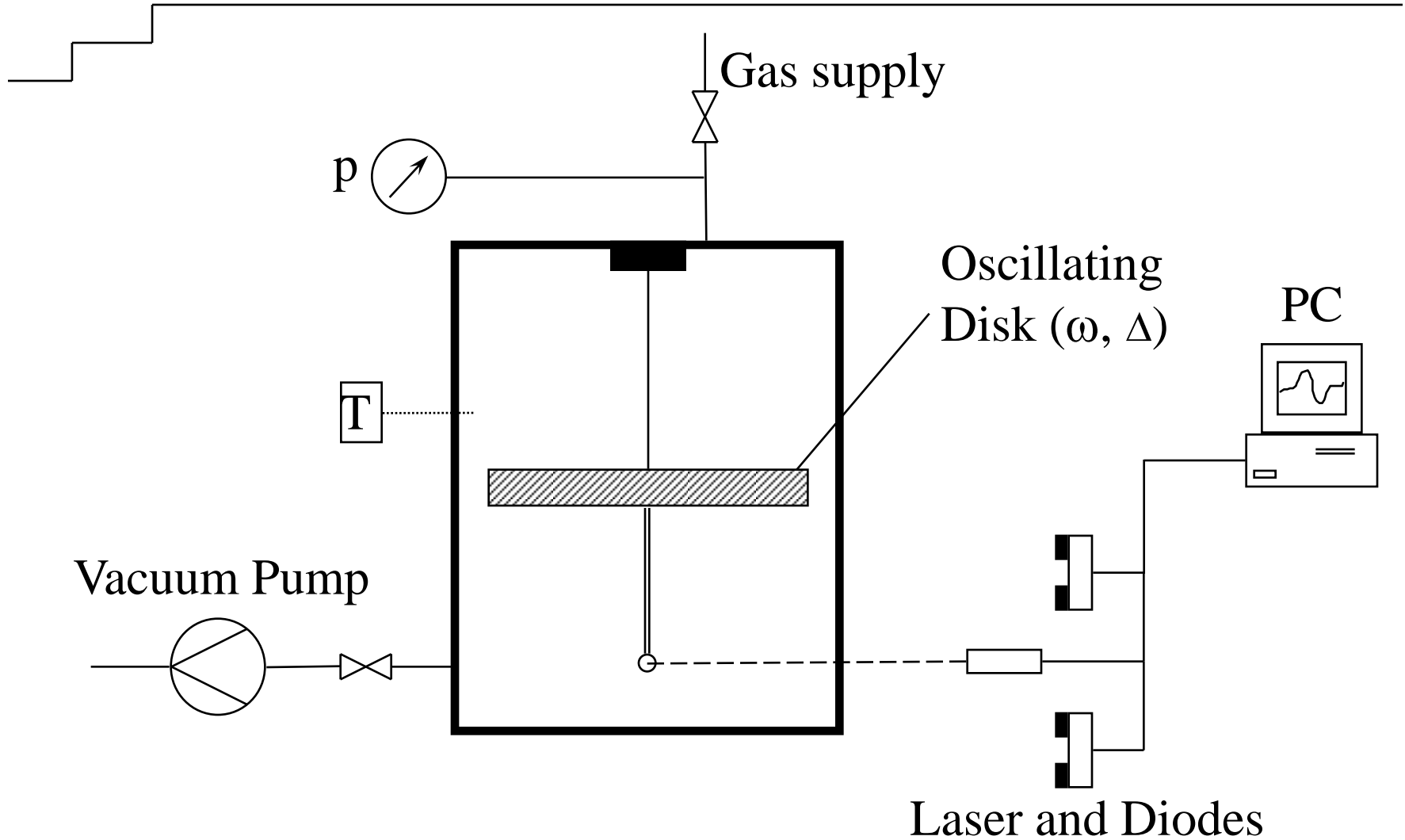


Coadsorption equilibria of  $\text{CO}_2 / \text{CH}_4$  at  $T = 293\text{K}$ ,  $y_{\text{CO}_2} = 20.4\% \text{ mol}$ ,  $y_{\text{CH}_4} = 79.6\% \text{ mol}$  on AC D47/3. Correlation by GAI:  $n_i = n_{i_\infty} (bp)^{\alpha_i} / [1 + (bp)^{\alpha_i}]$ ,  $i = \text{CO}_2, \text{CH}_4$

Comparison of experimental pros and cons of densimetric-gravimetric measurements (DGMs) and densimetric-volumetric measurements (DVMs) of binary gas adsorption equilibria without analyzing the sorptive phase.

Criterion	DGMs	DVMs
1. Equipment needed	Magnetic suspension balance (3 positions)	Spring balance (quartz), microbalance, magnetic suspension balance (2 positions)
2. Operation	sophisticated	fairly simple
3. Automation	sophisticated	fairly simple
4. Kinetics	can be observed	hardly observable
5. Activation of sorbent	inside the instrument i. e. controllable	outside the instrument i. e. often changed during transportation of sorbent to the instrument
6. Amount of sorbent needed	small ( $> 0.1$ g)	large (5 g – 100 g)
7. Wall adsorption	neglectable	may cause serious errors or uncertainties
8. Uncertainties of measurements	add up in pressure step-up experiments	add up more rapidly in pressure step-up experiments
9. Thermostatization	easily achievable	achievable, but takes more time





# Experimental Setup for Oscillometric Measurements of Gas Adsorption Equilibria



Ideal Pendulum  $m^s, m$

$$\frac{m}{m^s} = \frac{1 + \Delta_0^2 \left( \frac{\omega_0}{\omega_E} \right)^2}{1 + \Delta_E^2} - 1$$

Physical Pendulum  $m^*, m^s, m$

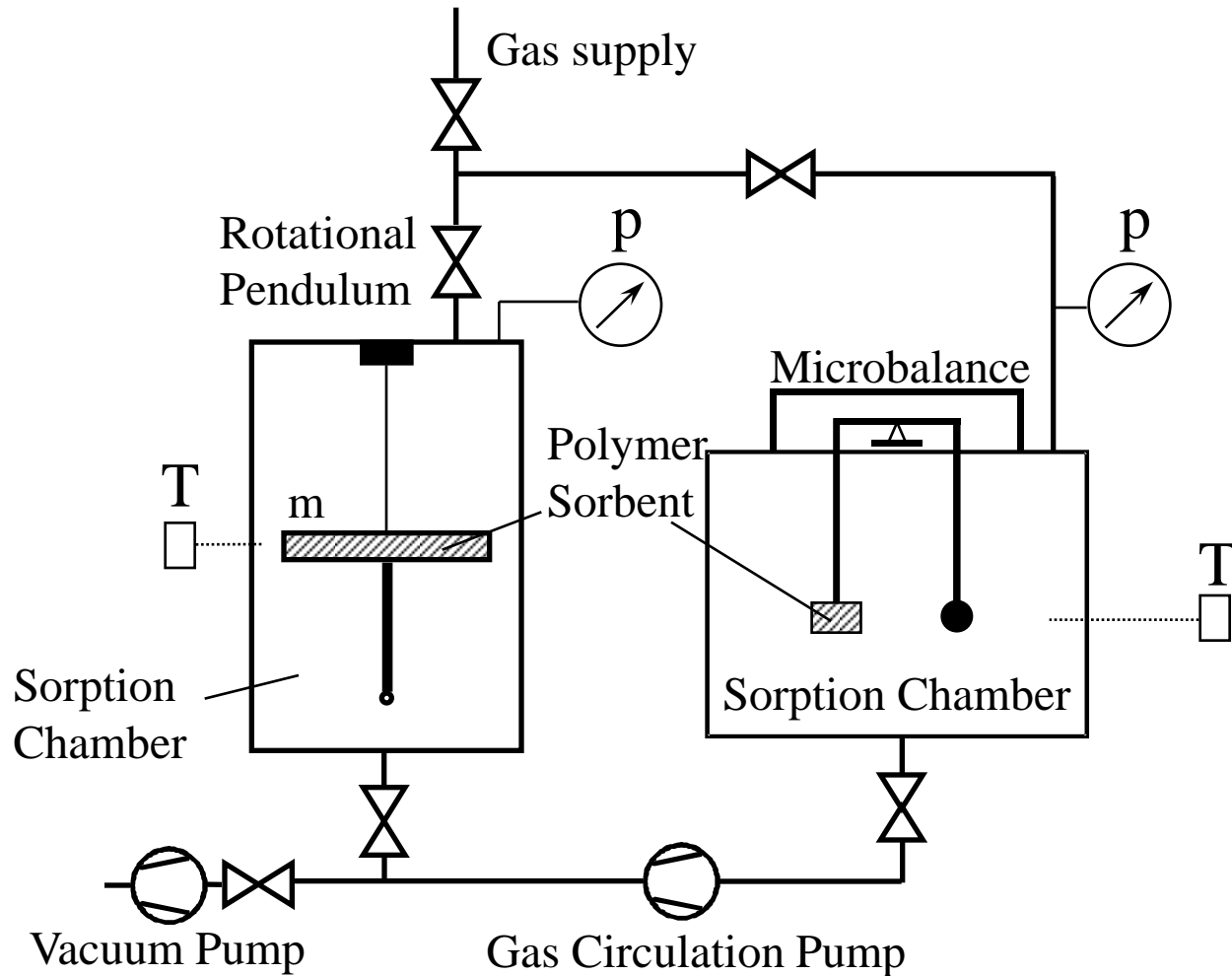
$$\frac{m}{m^s} = \frac{\frac{1 + \Delta_0^2 \left( \frac{\omega_0}{\omega_E} \right)^2}{1 + \Delta_E^2} - 1}{1 - \frac{\Delta_0 \omega_0}{\Delta^* \omega^*}}$$

$\omega^*, \Delta^*$  ... empty pendulum  $m^*$ , vacuum

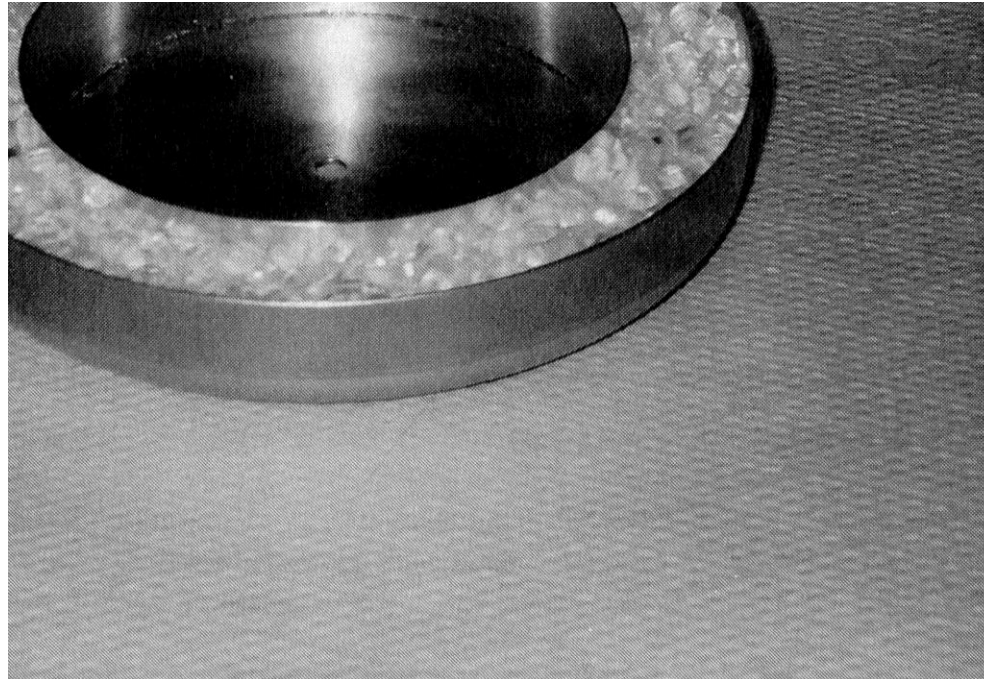
$\omega_0, \Delta_0$  ... pendulum and adsorbent  $m^*, m^s$ , vacuum

$\omega_E, \Delta_E$  ... pendulum, adsorbent, adsorbate  $m^*, m^s, m$ , gas

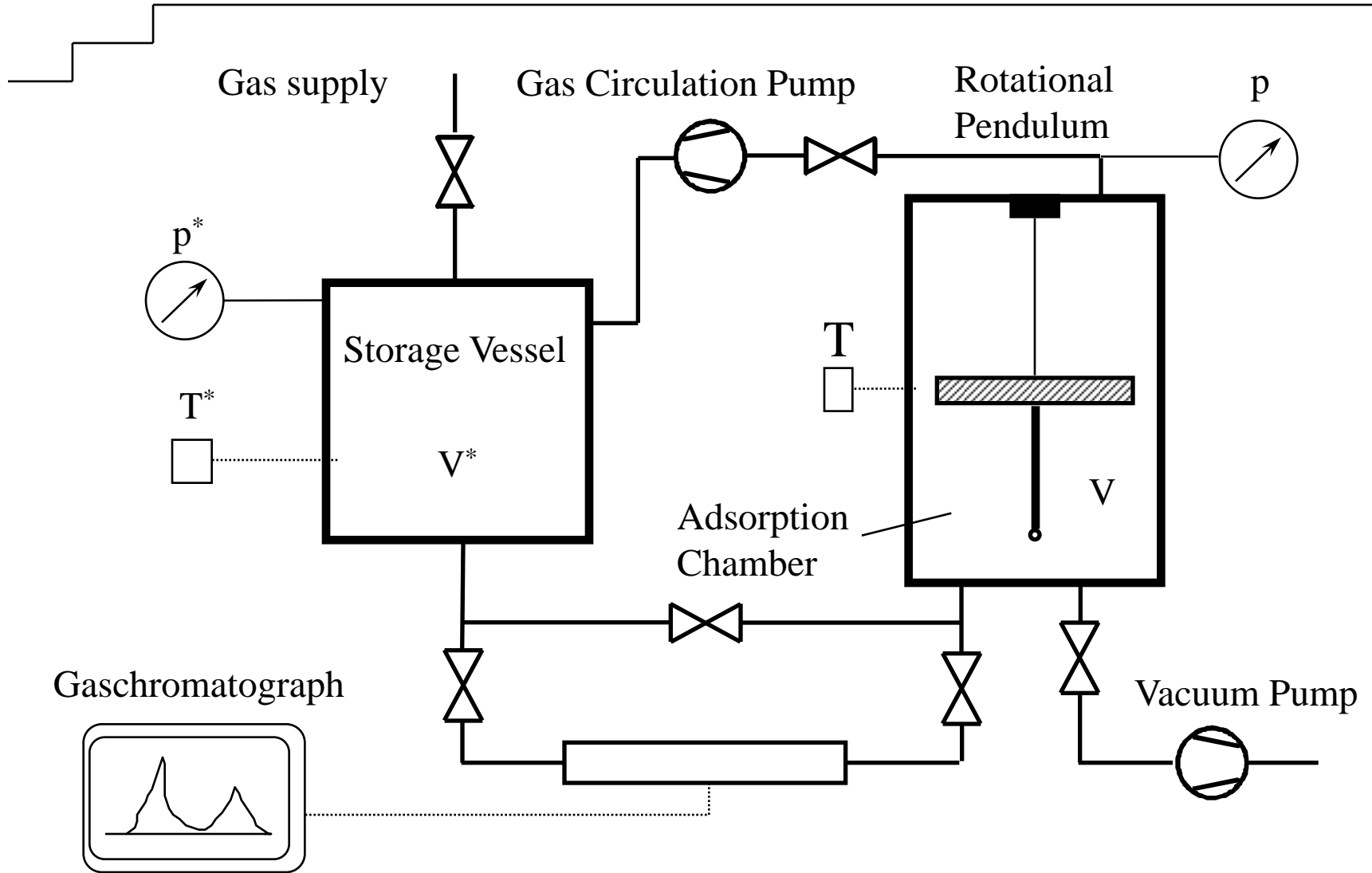
## Oscillometric Measurements of Gas Adsorption Equilibria. Theory



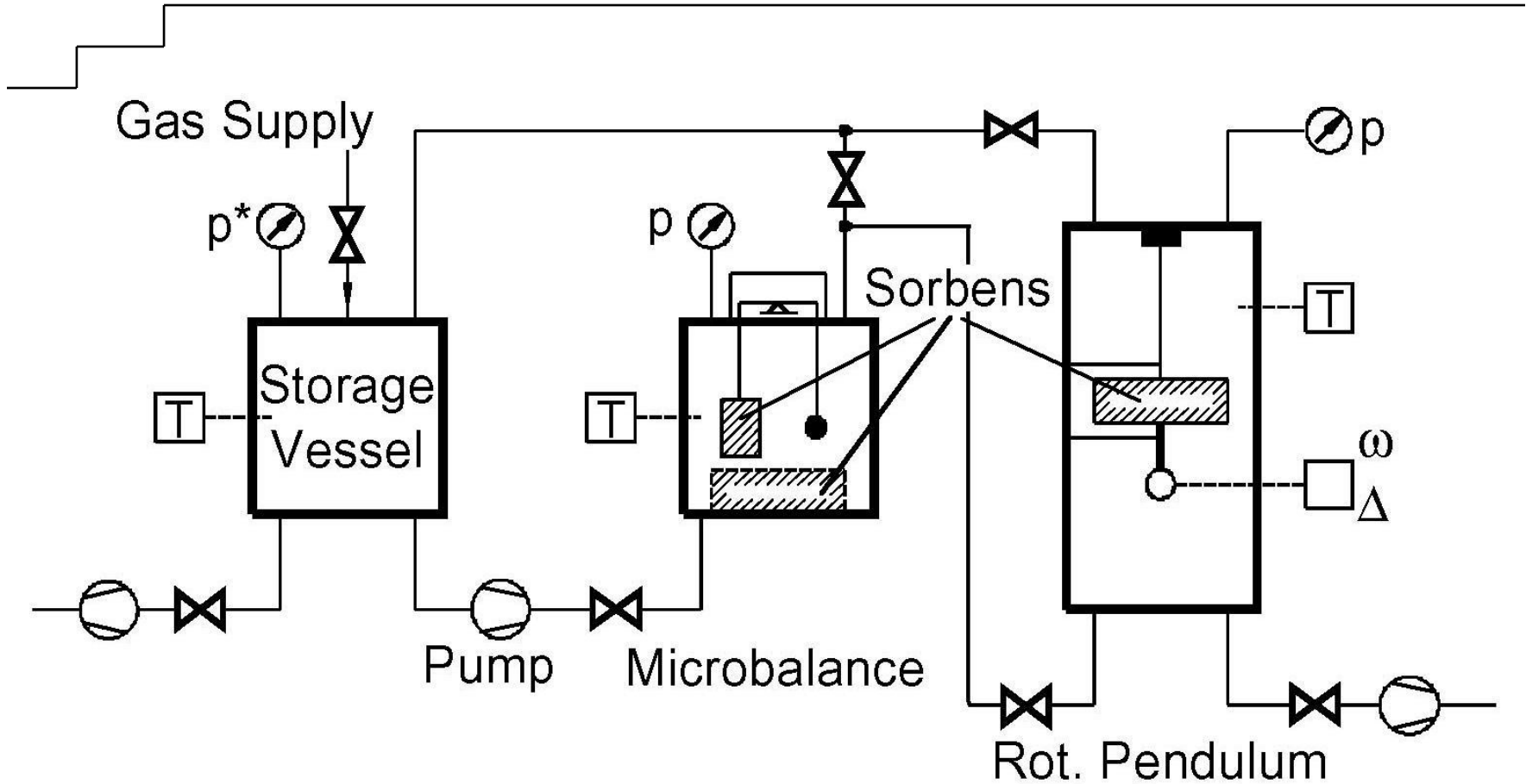
## Experimental Setup for oscillometric-gravimetric measurements



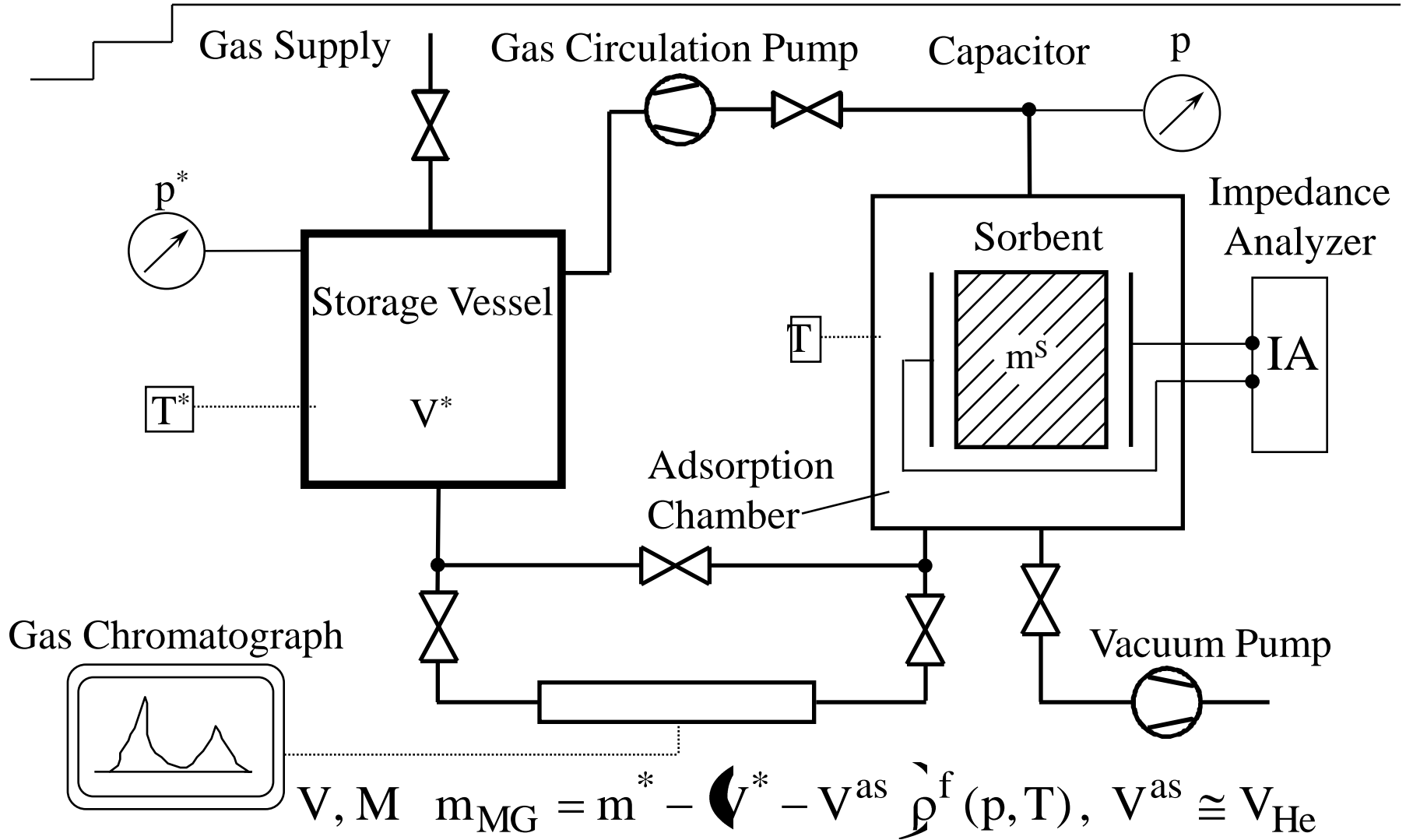
**Ring slit of rotational pendulum filled with polycarbonate pellets**



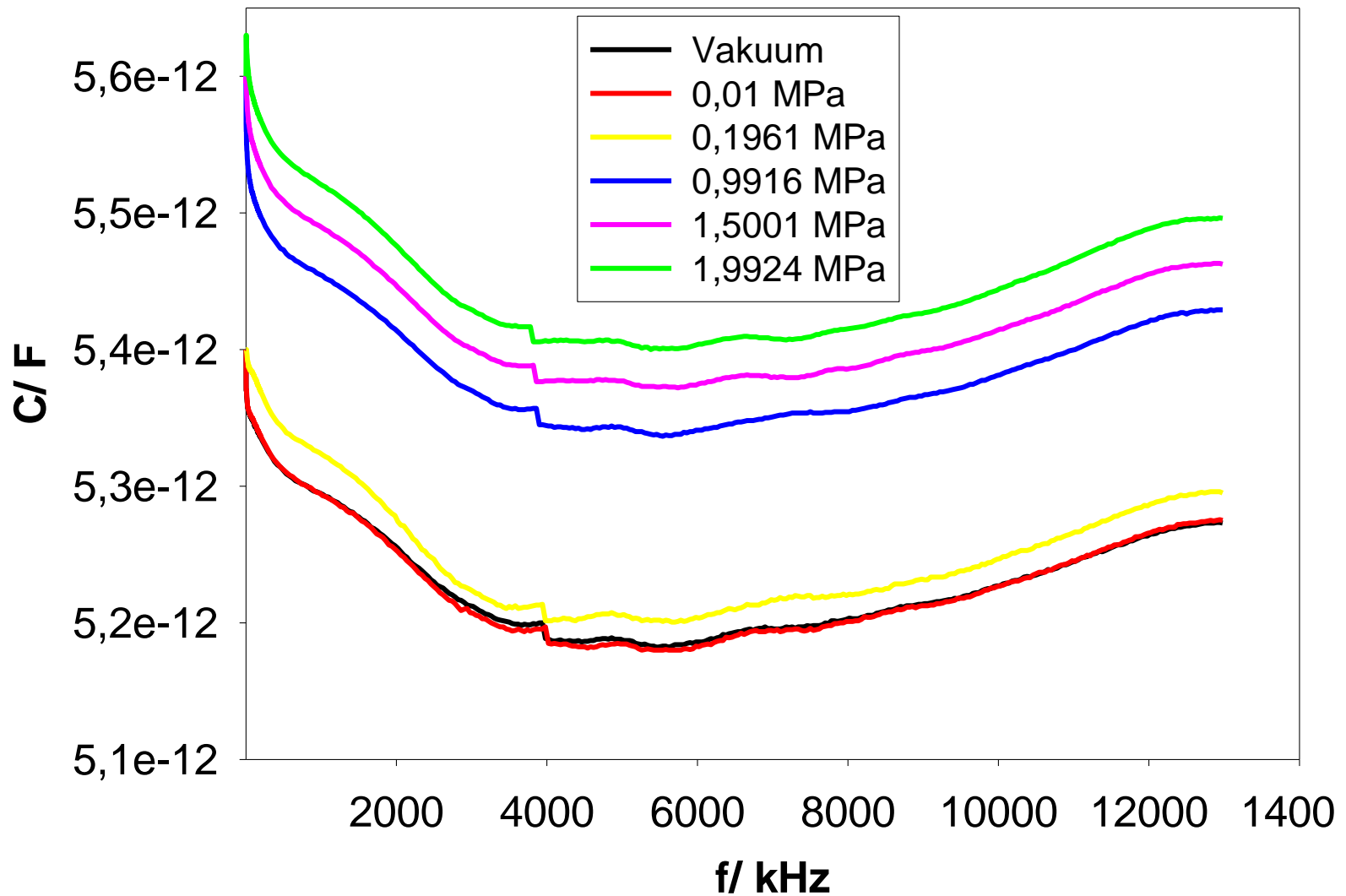
**Experimental Setup for oscillometric-volumetric measurements**



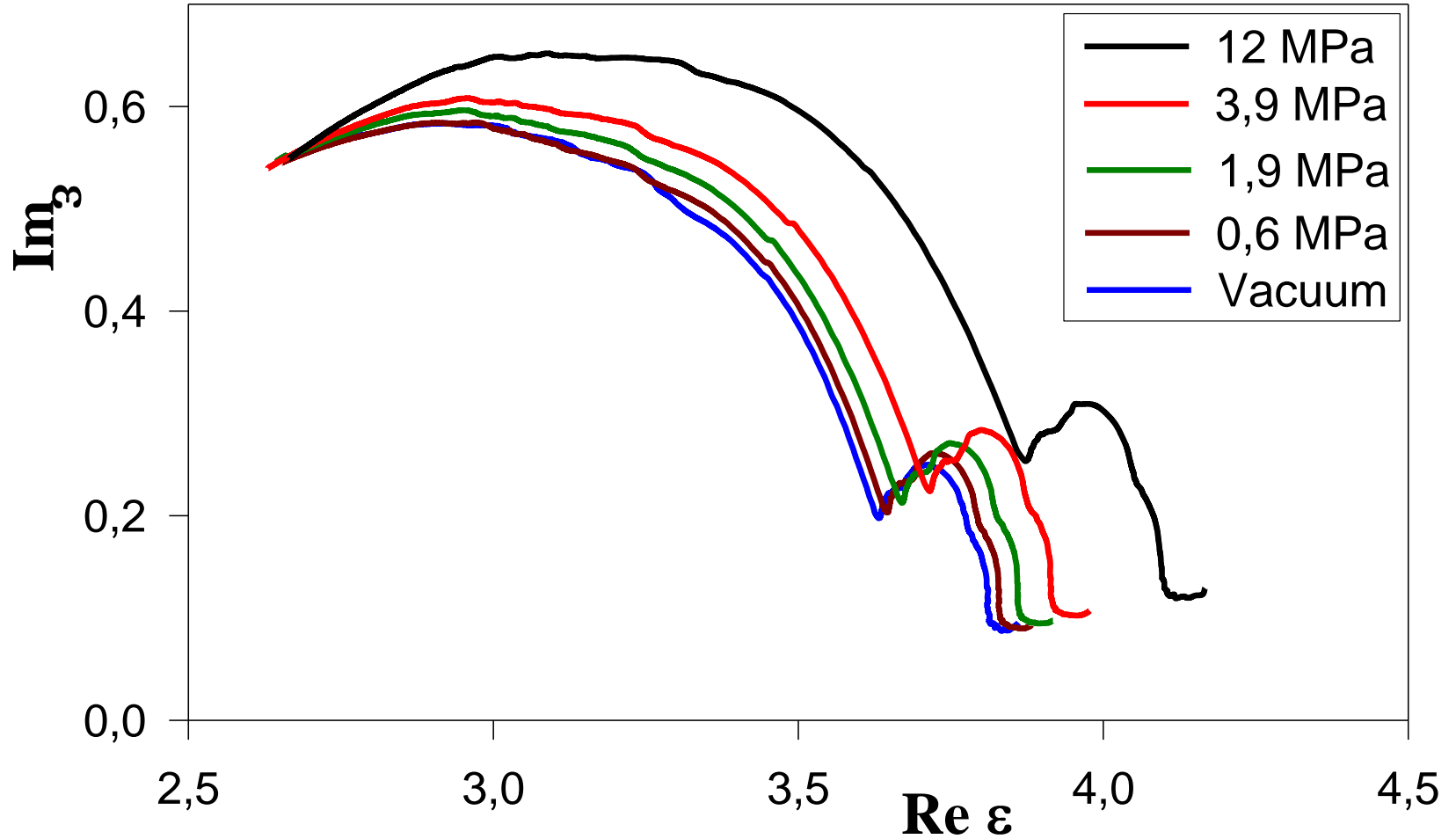
**Volumetric-gravimetric-oscillometric method (N=2).  
 Co(ad)sorption measurements in swelling sorbents  
 (polymers) without using a GC**



## Experimental setup for volumetric-dielectric measurements

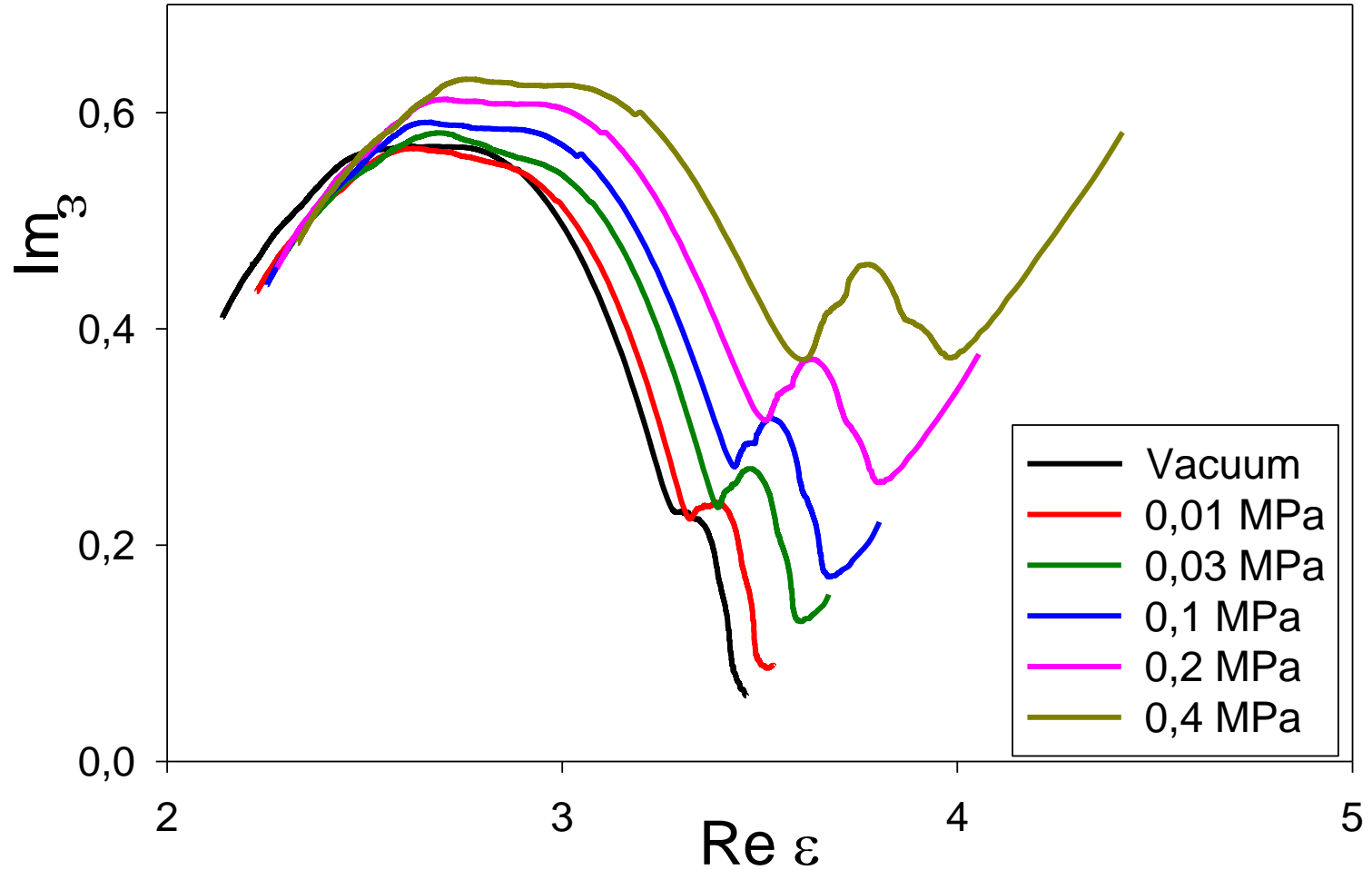


**Impedance spectra of CO<sub>2</sub> on zeolite (DAY), T=298K**

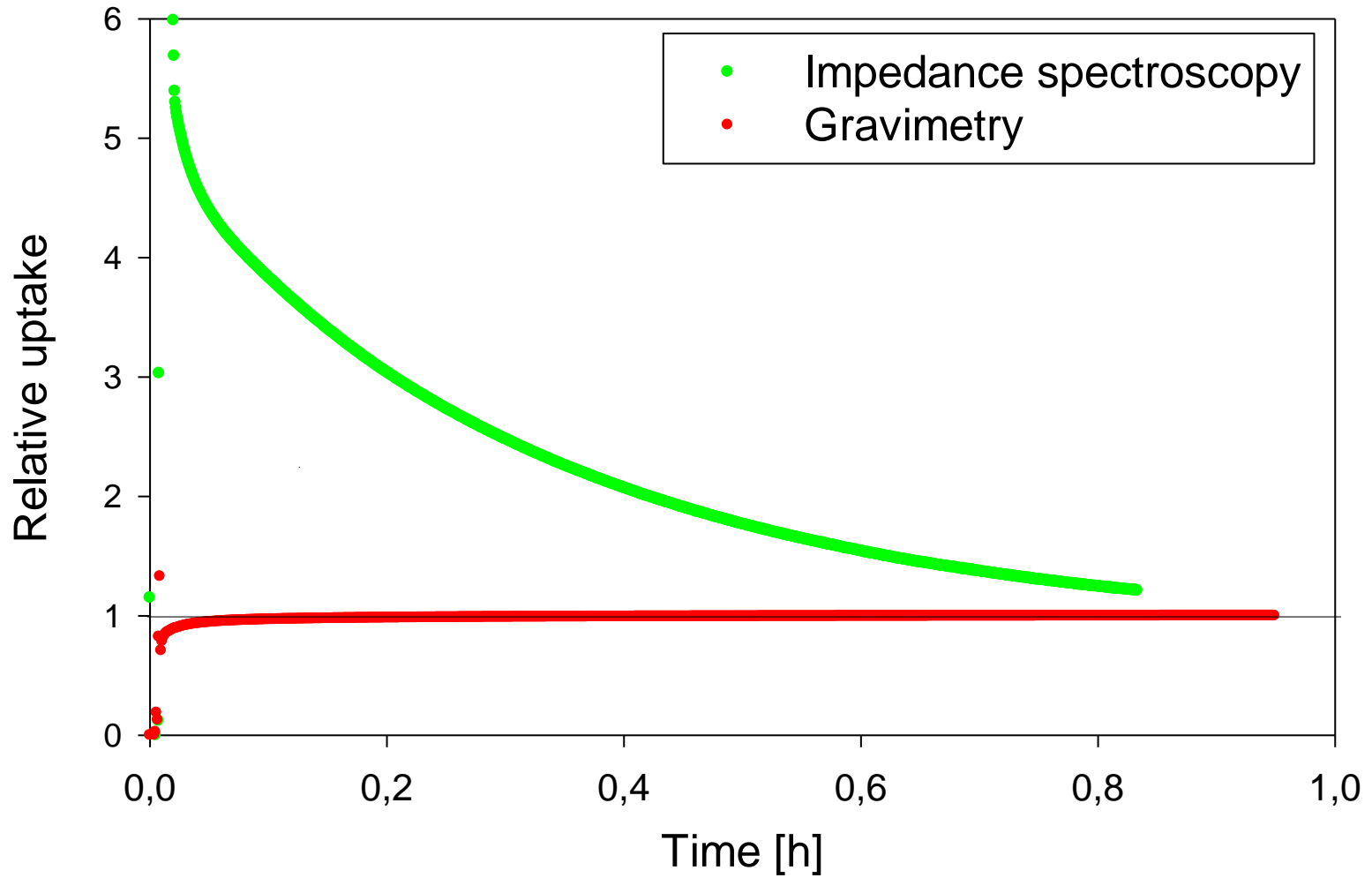


**Cole-Cole-Plot for system CO / MS 13X, T=298K**

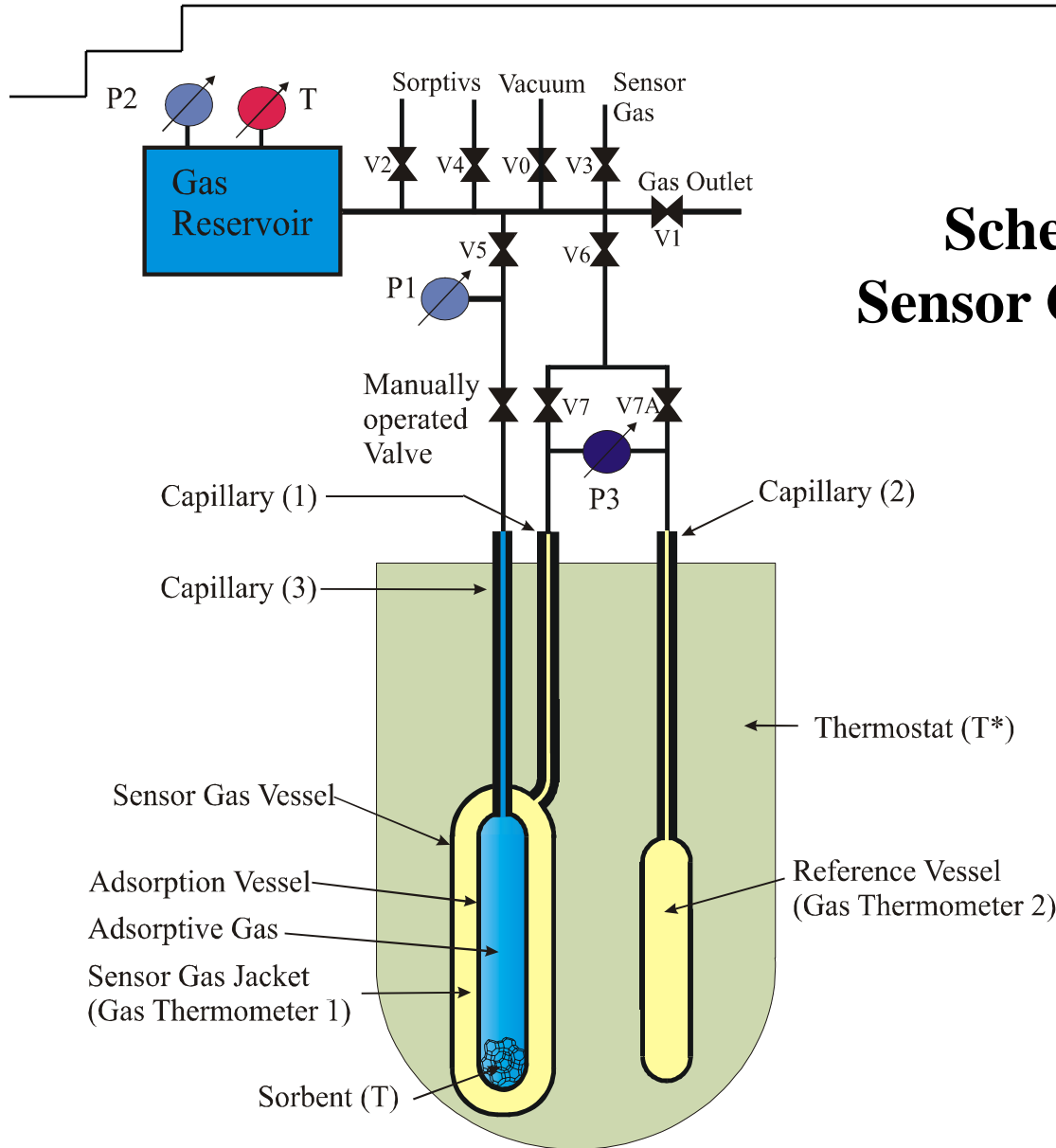




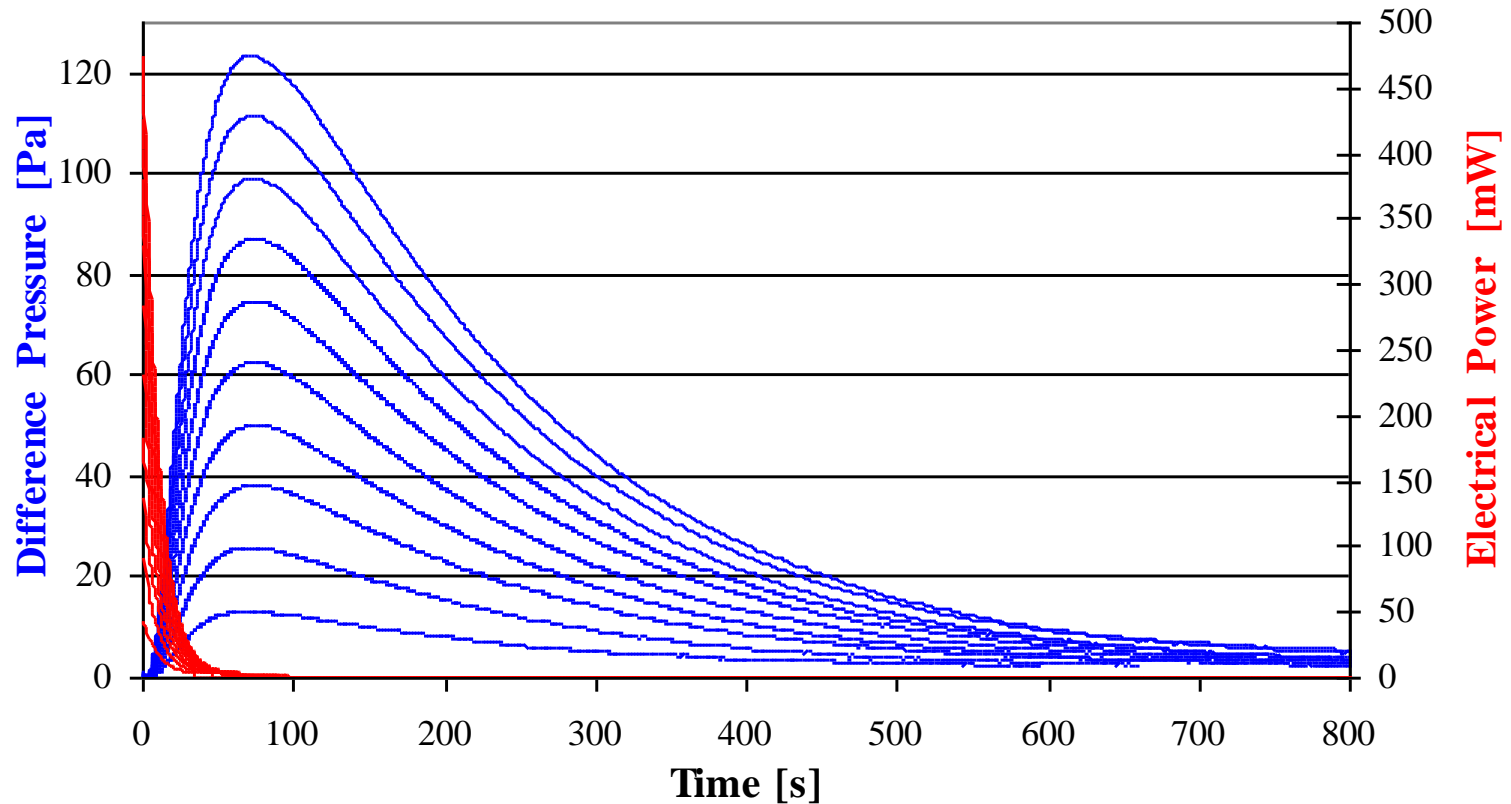
**Cole-Cole-Plot for system  $\text{H}_2\text{S}$  / MS 13X,  $T=298\text{K}$**



**Uptake curves of H<sub>2</sub>S on MS 13X, T=298K**



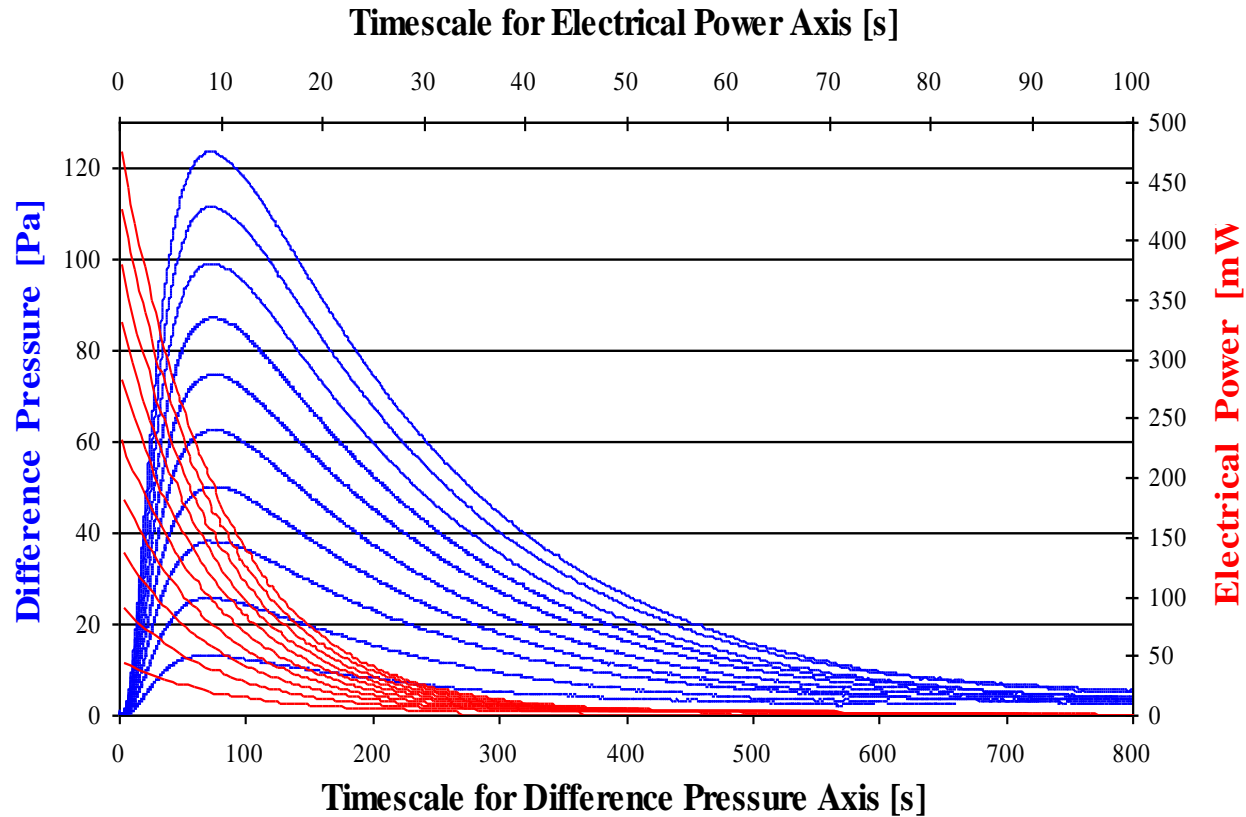
**Schematic diagram of a  
 Sensor Gas Calorimeter (SGC)**



**Calibration experiments in the SGC 0.5J to 5J**

**Sensor gas N<sub>2</sub> (1.6bar), T=298K, τ=10s**

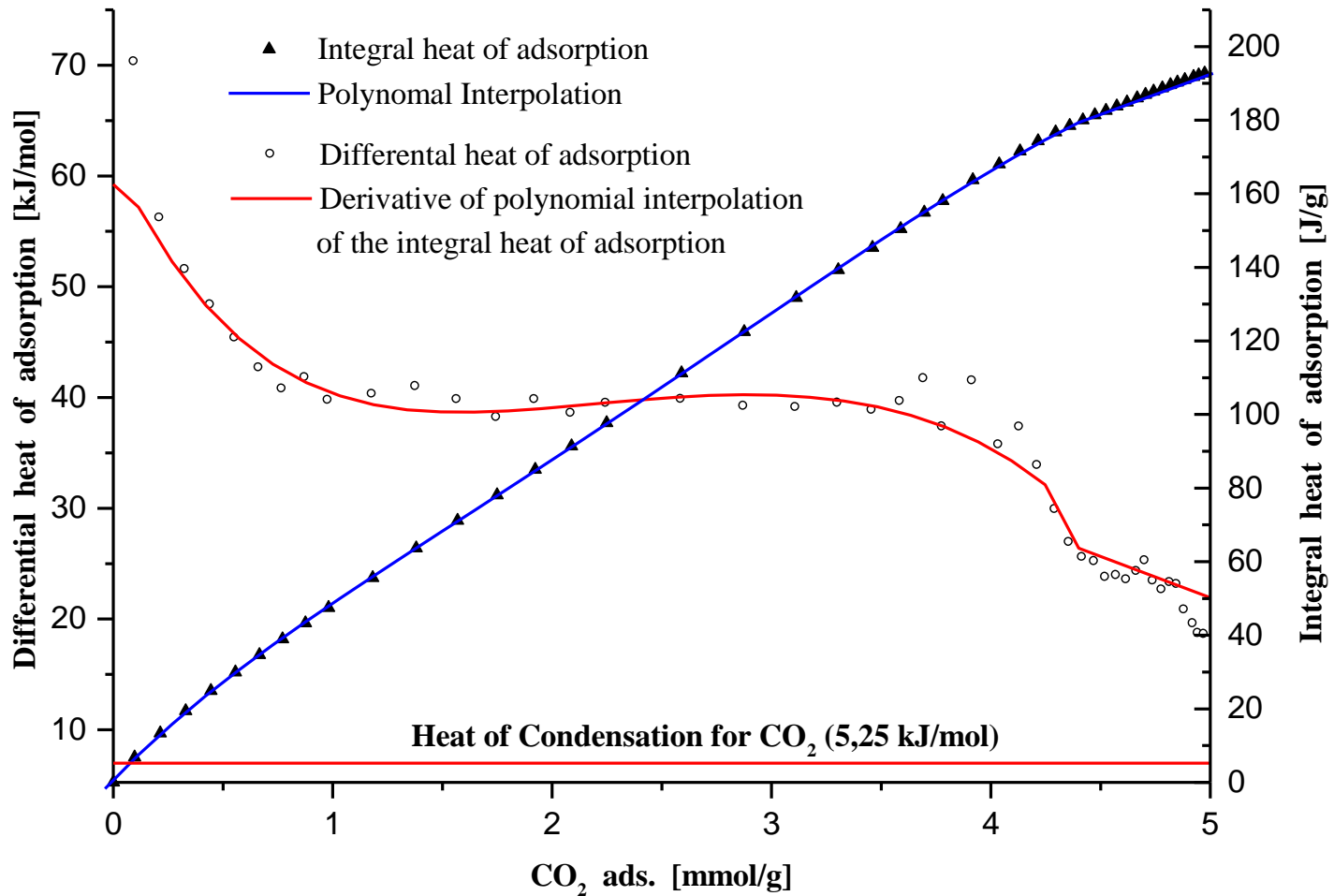
Ohmic heat release (red lines) → Pressure signal (blue lines)



**Calibration experiments in the SGC 0.5J to 5J**

**Sensor gas N<sub>2</sub> (1.6bar), T=298K, τ=10s**

Ohmian heat release (red lines) → Pressure signal (blue lines)



**Heat of adsorption for CO<sub>2</sub> / Na13X, T=298K**